Original Article

Removal of Formaldehyde from Aqueous Solutions by Advanced Oxidation processes: $UV/S_2O_8^{2-}/Fe^{2+}$ and $UV/S_2O_8^{2-}$

Abbas Khodabakhshi, Vida Hatami, Sara Hemati, Mehraban Sadeghi

Department of Environmental Health Engineering, Faculty of Health, Shahrekord University of Medical Sciences, Shahrekord, Iran

Abstract

Aims: This study aimed to comparatively investigate the efficiency of removal of formaldehyde using advanced oxidation process ultraviolet (UV)/S₂O₈^{2-/}Fe²⁺ and UV/S₂O₈²⁻ from aqueous solutions. **Materials and Methods:** In this experimental-laboratory study, the UV/S₂O₈^{2-/}Fe²⁺ processes were used to remove formaldehyde. UV radiation was provided by a low pressure (6 W) UV lamp. Effects of various factors including pH, different irradiation durations, different concentrations of iron ions, initial concentration formaldehyde, and persulfate concentration were evaluated. The remaining formaldehyde concentration in the samples was measured by spectrophotometer at 412 nm wavelength. **Results:** The results showed that in the UV/S₂O₈²⁻ method, the formaldehyde removal efficiency decreased with increasing pH from 3 to 9, while in the UV/S₂O₈^{2-/}Fe²⁺ method, the formaldehyde was increased, its removal efficiency decreased, and the highest formaldehyde removal rate was obtained in UV/S₂O₈²⁻ method at persulfate concentration of 100 mM. However, in the UV/S₂O₈^{2-/}Fe²⁺ method, the removal efficiency decreased with increasing concentration of persulfate to 100 mM. **Conclusion:** The results showed that the UV/S₂O8^{2-/}Fe²⁺ process was more efficient (87.57%) to remove formaldehyde at high concentrations. Therefore, it is recommended to study the efficiency of this process as one of the clean and environmentally friendly methods at full scale for real wastewater.

Keywords: Advanced oxidation process, formaldehyde, ultraviolet/persulfate/iron

INTRODUCTION

One of the most important challenges facing the world is the production of wastewater from various industries in the current century, which has resulted in severe environmental pollution. Meanwhile, some industries produce wastewater containing numerous hazardous compounds that necessitate paying attention to wastewater treatment. Formaldehyde is one of these contaminants.^[1,2]

Formaldehyde is widely used as an initial substance because of its high reactivity, sustainability, and low cost in industries such as synthetic resin manufacturing, cosmetic products, chemical and petrochemical industries, photography, adhesive manufacturing, paper production, fabric manufacturing, polyester fiber manufacturing, medical and pharmaceutical products, plastics, fiberglass, and petroleum industries and thereby enters the environment.^[3] The formaldehyde concentration in industrial wastewater is within the range of

Access this article online				
Quick Response Code:	Website: www.ijehe.org			
	DOI: 10.4103/ijehe.ijehe_25_20			

100–10,000 mg/l, and unfortunately, this substance can pose risks to aquatic ecosystems even at a concentration of <1 ppm.^[4] Formaldehyde compounds are leading among the 45 chemicals in the toxic substances list published by the US Environmental Protection Agency due to their specific properties, such as acute and chronic toxicity, harmful effects on humans' and living organisms' health.^[5] Given that this substance causes substantial toxicity and carcinogenicity effects, contamination with it results in irreparable damages, raising environmental concerns in today's world.^[6] Thus, the removal

Address for correspondence: Dr. Mehraban Sadeghi, Department of Environmental Health of Engineering, Faculty of Health, Shahrekord University of Medical Sciences, Shahrekord, Iran. E-mail: sadeghi@skums.ac.ir

This is an open access journal, and articles are distributed under the terms of the Creative Commons Attribution-NonCommercial-ShareAlike 4.0 License, which allows others to remix, tweak, and build upon the work non-commercially, as long as appropriate credit is given and the new creations are licensed under the identical terms.

For reprints contact: reprints@medknow.com

How to cite this article: Khodabakhshi A, Hatami V, Hemati S, Sadeghi M. Removal of formaldehyde from aqueous solutions by advanced oxidation processes: $UV/S_2O_8^{2-}/Fe^{2+}$ and $UV/S_2O_8^{2-}$. Int J Env Health Eng 2020;9:20.

Received: 01-04-2020, Accepted: 11-08-2020, Published: 31-12-2020

1

Khodabakhshi, et al.: Removal of formaldehyde by UV/S2Og2-/Fe2+ and UV/S2Og2- processes

of formaldehyde from sewage before discharging into the environment with an effective process is absolutely essential to preserve and control human health in the environment against adverse impacts caused by it.^[7] Nowadays, various processes, including absorption, chemical, and biological processes, are used to remove formaldehyde from aqueous environments.^[1] One of these efficient and flexible processes, which can be a suitable strategy for formaldehyde degradation and treatment, is the advanced oxidation process (AOP), which is considered to be the basis of the production of reactive free radicals. Over the past few decades, these processes have generally been used as an effective method to destroy and eliminate hazardous, persistent, and nondegradable pollutants in a variety of aquatic environments.^[8] Electro-Fenton, O₃/MgO/H₂O₂ and ultraviolet (UV)/H₂O₂ are three of the processes used to remove formaldehyde.^[9] In AOPs, hydroxyl radical (OH) and sulfate radical (SO4⁻) can be generated by combination of strong oxidants (H_2O_2, O_2) with activators (transition metals), ultrasound irradiation, and UV. These radicals are powerful nonselective oxidizing agents that degrade organic pollutants.^[1]

The limitations of these methods are high consumption of energy in Electro-Fenton method, high cost of operation of O₂/MgO/ H₂O₂ method, and the complexity of commissioning and high cost of UV/H₂O₂ method. One of the effective technologies for treatment of water and industrial effluents is persulfate with oxidation potential of 2.01 V among all the oxidants used in AOPs, which has attracted widespread attention and generally indicates promising results for the removal of chemical contaminants.^[10] One of the characteristics that distinguish persulfate from other oxidants is high water solubility, relatively low cost, comparatively more stability and consequently more pollutant degradation, easy maintenance, and better transportation.[11] Despite all the advantages of persulfate, its reaction with the pollutants is slow and a catalyst is needed to accelerate the reaction so that persulfate can be activated.^[12] Several methods are used to activate persulfate, including intermediate metals, ozone, microwave, ultrasound waves, and UV radiation, whose final product is sulfate radical with a potential of oxidation of 2.6 V which is much higher than potential of oxidation of hydrogen peroxide (1.76 V).[13] The general reaction between persulfate and iron as one of the intermediate metals is presented in Equations (1) and (2). The addition of Fe^{2+} according to Equation (2) can increase the efficiency and synergy effect in the decomposition of target compounds.

$$S_2O_8^{2-} + hv \rightarrow 2SO_4 \tag{1}$$

$$Fe^{2+} + S_2O_8^{2-} \rightarrow Fe^{3+} + SO_4^{2+} + SO_4^{2-}$$
 (2)

The purpose of this study was to compare the activation of persulfate with UV light alone and along with Fe^{2+} ions to produce sulfate radical and thus remove high concentrations of formaldehyde from water. Besides that, effective factors including persulfate dosage, bivalent iron ion content, irradiation time, and solution pH for removal of formaldehyde using these two methods were investigated.

MATERIALS AND METHODS Materials

A formalin solution containing 37% formaldehyde and the deionized water was used to prepare formaldehyde solutions. Formalin, sodium persulfate (Na₂S₂O₈ \geq 99%), sulfuric acid (H₂SO₄), sodium hydroxide (NaOH \geq 99.8%), and iron sulfate (FeSO₄.7H₂O) solutions and other chemicals and reagents were purchased from Merck Co. (Germany).

As illustrated in Figure 1, all experiments were performed on a cylindrical reactor made of quartz with an inner diameter of 5 cm and a height of 25 cm. There was a UV-C lamp at wavelength of 254 nm and a power of 6 w (middle range) at the center of the reactor. A magnetic stirrer was used at 150 rpm to mix the reactor contents. To prevent the temperature rise, the chemical reactor was placed in a cylindrical container equipped with an inlet and outlet water flow, and the permeation of ambient light into the reactor was prevented by the aluminum coating. In this study, the effects of all parameters were investigated at optimal pH. Therefore, the effect of pH at 3, 5, 7, and 9 was initially assessed to determine the optimal pH for the removal efficiency of formaldehyde using the UV/S₂O₈²⁻/Fe²⁺ and UV/S₂O₈²⁻ processes.

Sulfuric acid and sodium hydroxide solutions at 0.1 M were used to adjust the pH of the aqueous solution, and the Metrohm pH meter was used to measure it. After determining the optimal pH, the effect of sodium persulfate concentration at 10, 25, 50, and 100 mM; initial formaldehyde concentration at 1000, 2500, 5000, and 10,000 mg/l; and the exposure intervals of 0–96 min were examined in the UV/S₂O₈^{2–} method. As well, the effect of sodium persulfate parameters at 25, 50, and 100 mM; formaldehyde concentration at 5000, 7500, and 10,000 mg/l; iron sulfate at 12, 14, 18, and 20 mM; and the exposure time of 0–60 min were investigated in the UV/S₂O₈^{2–}/Fe²⁺ method. All tests were performed in triplicate to ensure the reliability and evaluation of the standard deviation. At the completion of each step, the residual formaldehyde amount was determined using the Hantzsch method and the UNICO spectrophotometer

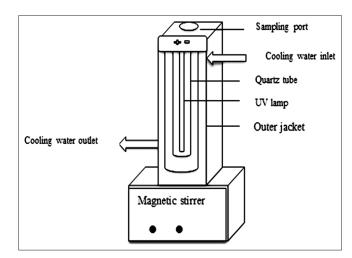


Figure 1: Schematic of the present study

apparatus (2100UV-Vis) at 412 nm wavelength.^[14,15] In this study, the experiments were designed according to full factorial design. One-way ANOVA was used for result interpretation. Statistical analyses were performed by IBM Corp Chicago SPSS version 23.0. P < 0.05 was considered as the level of significance.

RESULTS

pH

The effect of pH on the efficiency of formaldehyde removal is illustrated in Figure 2. In the UV/S $_{2}O_{8}^{2-}$ method, the formaldehyde removal efficiency decreased with increasing pH from 3 to 9, while in the UV/S₂O₈²⁻/Fe²⁺ method, formaldehyde removal efficiency increased with increasing pH, so that the highest removal efficiency was obtained at pH = 9.

Figure 2 shows changes in formaldehyde removal efficiency versus pH (in the UV/S2O82- method: formaldehyde initial concentration = 1000 mg/l; exposure time = 48 min; PS = 50 mM; and in the UV/S₂O₂²⁻/Fe²⁺ method: formaldehyde initial concentration = 5000 mg/l; exposure time = 60 min; $PS = 50 \text{ mM}; Fe^{2+} = 20 \text{ mM}).$

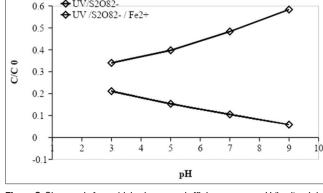
Effect of formaldehyde initial concentration, persulfate, and iron concentration

The effect of formaldehyde initial concentration on the efficiency of UV/S₂O₈²⁻ and UV/S₂O₈²⁻/Fe²⁺ in formaldehyde removal is illustrated in Figures 3 and 4. In Figure 3, the removal rate at 48 min at 1000, 2500, 5000, and 10,000 mg/l was 94.08%, 83.41%, 69.73%, and 46.16%, respectively. The same results are shown in Figure 4, except that the highest removal rate at 10 min and at 5000, 7500, and 10,000 mg/l was obtained 83.55%, 79.50%, and 77.28%, respectively. Figures 5 and 6 illustrate the rate of formaldehyde removal in response to the reaction time in the $UV/S_2O_2^{2-}$ and $UV/S_2O_8^{2-}/Fe^{2+}$ methods at initial concentrations of 1000 and 5000 mg/l of formaldehyde, respectively. A comparison of Figures 5 and 6 is presented in Table 1. Figure 7 illustrates the rate of formaldehyde removal compared to time at different initial concentrations of iron in the UV/S₂O₂²⁻/Fe²⁺ method, where the removal efficiency for iron concentrations of 12, 14, 18, and 20 mM was 83.55%, 85.94%, 87.18%, and 89/75%, respectively.

DISCUSSION

Effect of pH

The type and number of radicals produced in the AOPs are the most important factors for the pH changes of the environment in the decomposition of organic compounds in these processes.^[16] As illustrated in Figure 2, it can be concluded that the removal efficiency of formaldehyde in the $UV/S_2O_8^{2-}$ method was higher at acidic pH, which can be attributed to the higher rate of sulfate radical produced at pH = 3.^[17] In fact, this is due to the presence of hydrogen ions in the acidic environments that serve as precursors to hydrogen



◆UV/S2O82-

Figure 2: Changes in formaldehyde removal efficiency versus pH (in ultraviolet/ $S_{o}O_{o}^{2-}$ method: Formaldehyde initial concentration = 1000 mg/l; exposure time = 48 min; PS = 50 mM; and in the ultraviolet/S₂O₈²⁻/Fe²⁺ method: Formaldehyde initial concentration = 5000 mg/l; exposure time = 60 min; $PS = 50 \text{ mM}; Fe^{2+} = 20 \text{ mM})$

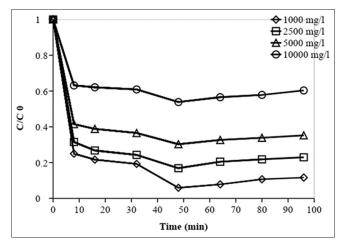


Figure 3: Changes in formaldehyde removal efficiency versus exposure time for different initial formaldehyde concentrations in ultraviolet/ $S_{2}O_{2}^{2}$ -method (PS = 100 mM; pH = 3)

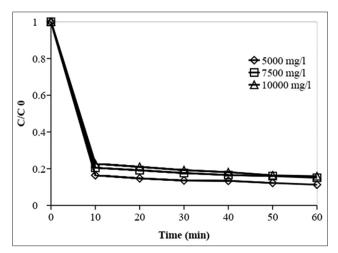
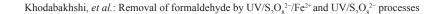


Figure 4: Changes in formaldehyde removal efficiency versus exposure time for different initial formaldehyde concentrations in the ultraviolet/S₂O₂²⁻/Fe²⁺ method (PS = 50 mM; Fe²⁺=12 mM; pH = 9)



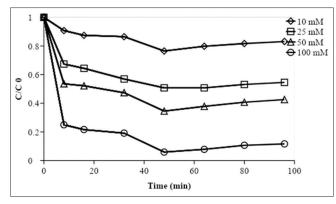


Figure 5: Changes in formaldehyde removal efficiency versus exposure time for different concentrations of persulfate in the ultraviolet/ $S_0O_a^{2-}$ process (formaldehyde initial concentration = 1000 mg/L; pH = 3)

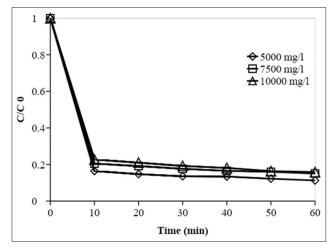


Figure 6: Changes in formaldehyde removal efficiency versus exposure time for different concentrations of persulfate in the ultraviolet/ $S_2O_8^{2-}/Fe^{2+}$ process (initial concentration of formaldehyde = 5000 mg/l; Fe²⁺ = 12 mM; pH = 9)

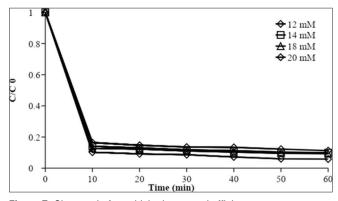


Figure 7: Changes in formaldehyde removal efficiency versus exposure time for different concentrations of iron in the ultraviolet/ $S_2 O_8^{2-}/Fe^{2+}$ process (initial concentration of formaldehyde = 5000 mg/l; PS = 50 mM; pH = 9)

radicals. Then, the radicals form through the reaction with oxygen in the solution that finally leads to the formation of radicals.^[18] In the study of Raeisivand *et al.*, the maximum

Table 1: Comparison of two methods of ultraviolet/S2082	-			
and ultraviolet/ $S_2 O_8^{2-}/Fe^{2+}$ in optimal conditions				

Initial concentration	UV/S ₂ 0 ₈ ^{2-*}		UV/S ₂ O ₈ ²⁻ /Fe ^{2+**}		
of formaldehyde (mg/L)	Persulfate concentration (mM)				
	50 (%)	100 (%)	50 (%)	100 (%)	
1000	64.81	94.08	-	-	
5000	38.17	69.73	87.57	84.79	

*Optimal conditions of method 1: Initial concentration of formaldehyde=1000 mg/L; pH=3, **Optimal conditions of method 2: Initial concentration of formaldehyde=5000 mg/L. UV: ultraviolet

catechol degradation efficiency was obtained at pH = 2 that is consistent with the present study.^[19] The results also show that the amount of formaldehyde removal was higher at pH = 9 in the UV/S₂O₈²⁻/Fe²⁺ method, which is due to increased hydroxide concentration and subsequent formation of sulfate and hydroxide radicals (Equations 3 and 4).^[20,21] Consistent with our results, Haddad *et al.* reported that in the UVC/VUV photoreactor process, the OHs were produced at the optimal pH of 7.^[1] Our obtained results are also in agreement with the study of Guimarães *et al.* at pH 6–7.^[4]

$$SO4^- + OH^- \rightarrow SO_4^{2-} + OH \tag{3}$$

$$SO4^{-} + OH \rightarrow HSO_4^{-} + 0.5O_2$$
 (4)

Effect of formaldehyde initial concentration

The same results are shown in Figure 4, except that the highest removal rate at the time of 10 min and at concentrations of 5000, 7500, and 10,000 mg/l was obtained 83.55%, 79.50%, and 77.28%, respectively. In addition, the removal efficiency increases with increasing reaction time to 60 min. However, this increase initially had a uniform slope, and then, there was no significant difference between the removal efficiency at 10 min and 60 min, so it can be concluded that if the UV/S₂O₈²⁻/Fe²⁺ method is applied for removal of formaldehyde in comparison with the UV/S₂O₈²⁻ method, it is not necessary to increase the time and the volume of the reactor. The results drawn from Figures 3 and 4 show that the increase of formaldehyde concentration in both methods reduces the removal efficiency of formaldehyde. Increasing the organic pollutant concentration reduces the removal efficiency for two main reasons: (1) the exposure rate decreases with increasing formaldehyde in constant amounts of sulfate radical and (2) the increase of the formaldehyde concentration will produce more oxidation-related by-products that act as a competitor for formaldehyde and will consume more amounts of sulfate radical.[4,22] Besides that, according to Figure 4 and the UV/S₂O₂²⁻/Fe²⁺ method, the effect of the initial formaldehyde concentration on the removal rate is much lower than that in the first method, so that it can be even ignored with increasing reaction time.

Effect of persulfate concentration

According to our results [Figure 5], the formaldehyde

removal efficiency significantly increased with the increase of persulfate concentration from 10 mM to 100 mM. As illustrated in Figure 5, the highest removal rate was obtained at all concentrations of persulfate at 48 min, so that the highest removal rate of formaldehyde at 100 mM of persulfate was 94.08%. In AOPs, one of the effective factors for the removal of organic compounds is the type and concentration of oxidizing material.^[23] As the oxidizing material increases, the reaction rate and the amount of formaldehyde removal will increase. The reaction rate and removal value increase due to the increased production of free radicals at higher concentrations of oxidants.^[16,24]

In a study by Wang *et al.* on the removal of humic acid using the ultrasonic/persulfate process, increasing the concentration of persulfate from 10 to 100 mM increased the removal efficiency of humic acid, which is consistent with the results of the present study.^[25] The study of Gao *et al.* showed that increasing the sodium persulfate concentration increased the removal of sulfamethazine and fluorophenol from water by UV/persulfate process.^[26,27]

As illustrated in Figure 6, with the addition of iron, the highest removal value was obtained at 50 mM concentration of persulfate and the highest change was observed in exposure time of 10 min with a removal efficiency of 83.55%, while the increase in exposure time to 60 min did not have any significant effect on increase of formaldehyde removal.

A comparison of Figures 5 and 6 is presented in Table 1. As seen, the highest formaldehyde removal rate was obtained in UV/S₂O₈²⁻ method at persulfate concentration of 100 mM. However, in the UV/S₂O₈²⁻/Fe²⁺ method, the removal efficiency decreased with increasing concentration of persulfate to 100 mM, and thus, sulfate radical production increased, because according to Equation (3), with increasing concentration of sulfate radical, this compound acts as an absorbent of the same compound and also reacts with persulfate in accordance with Equation (4) and produces sulfate anion, both of which result in the loss of sulfate radical and reduce the efficiency of removal.^[28]

$$SO_{4}^{-} + SO_{4}^{-} \rightarrow S_{2}O_{8}^{2-}$$

$$(4)$$

$$SO_{4}^{-} + SO_{4}^{2-} \rightarrow SO_{8}^{-+} + SO_{4}^{2-}$$

$$(5)$$

$$SO_4^{-} + S_2O_8^{-2-} \rightarrow SO_4^{-} + S_2O_8^{-2-} \tag{5}$$

Guo *et al.* and Saien and Asgari obtained similar results regarding the removal of quinoline in the microwave/ persulfate process for the removal of tetrabromobisphenol and iron/copper/UV/persulfate, respectively.^[29-31] The rate of formaldehyde removal in the UV/S₂O₈^{2–}/Fe²⁺ method was significantly higher than that of UV/S₂O₈^{2–} method in the initial concentration of formaldehyde equal to 5000 mg/l and both concentrations of persulfate. According to Equation (2), this shows that iron as an auxiliary agent has an increased effect on the production of sulfate radical.

Effect of iron concentration

The highest removal rate occurred at the exposure time of 10 min

in this case. Iron, as already mentioned, plays an important role in the production of sulfate-free radicals, so that increasing iron ion increases the production of SO_4^- and therefore increases the removal efficiency (Equations 5 and 6).^[32,33] Zhao *et al.* obtained similar results in a study on the removal of 4,1-dioxane.^[30,34]

$$S_{2}O_{8}^{2-} + Fe^{2+} \rightarrow Fe^{3+} + SO_{4}^{-} + SO_{4}^{2-}$$
(5)
SO4⁻ + Fe²⁺ \rightarrow Fe³⁺ + SO₄⁻ (6)

The present study indicated that the removal efficiency of formaldehyde depended on a variety of factors including pH, concentration of iron as an oxidant, persulfate concentration, and the initial concentration of the formaldehyde. The best formaldehyde removal efficiency (5000 mg/L) by UV/ $S_2O_2^{2-}$ process was 69.73% that was obtained at pH = 3, time = 48 min, and persulfate concentration of 100 mM. However, the application of UV/S₂O₈²⁻/Fe²⁺ process brought about the 87.57% removal of formaldehyde at 50 mM of persulfate concentration within 60 min at optimum solution pH of 7. From these observations, it can be concluded that the UV/S₂O₂²⁻/Fe²⁺ process is more efficient to remove high concentrations of formaldehyde from chemical and petrochemical industry wastewater. It is, therefore, recommended to study the efficiency of this process as one of the clean and environmentally friendly methods at full scale for real wastewater.

Acknowledgments

The authors are grateful to the Deputy of Research and Technology of Shahrekord University of Medical Sciences (SKUMS) for financial support and laboratory assistance of the Department of Environmental Health and Engineering, School of Health, SKUMS (ethics Code: IR.SKUMS.REC.1395.113).

Financial support and sponsorship

This study was financially supported by Shahrekord University of Medical Sciences, Shahrekord, Iran.

Conflicts of interest

There are no conflicts of interest.

REFERENCES

- Haddad FA, Moussavi G, Moradi M. Advanced oxidation of formaldehyde in aqueous solution using the chemical-less UVC/VUV process: Kinetics and mechanism evaluation. J Water Process Eng 2019;27:120-5.
- Parvaresh V, Hashemi H, Khodabakhshi A, Sedehi M. Removal of dye from synthetic textile wastewater using agricultural wastes and determination of adsorption isotherm. DesalinWater Treat 2018;111:345–350.
- Kowalik P. Chemical pretreatment of formaldehyde wastewater by selected advanced oxidation processes (AOPs). Chall Mod Technol 2011;2:42-48.
- Guimarães JR, Farah CR, Maniero MG, Fadini PS. Degradation of formaldehyde by advanced oxidation processes. J Environ Manage 2012;107:96-101.

Khodabakhshi, et al.: Removal of formaldehyde by UV/S2O22/Fe2+ and UV/S2O22 processes

- Yazdanbakhsh AR, Eslami A, Najafi A. Performance of aerobic sequencing batch reactor (SBR) for formaldehyde removal from synthetic wastewater. Iran J Health Environ 2013;6:233-42.
- Pereira NS, Zaiat M. Degradation of formaldehyde in anaerobic sequencing batch biofilm reactor (ASBBR). J Hazard Mater 2009;163:777-82.
- TrivediJ D, Crosse J, Tanti J, Cass AJ, Toghill KE. The electrochemical determination of formaldehyde in aqueous media using nickel modified electrodes. Sens Actuators B Chem 2018;270:298-303.
- Moussavi G, Pourakbar M, Aghayani E, Mahdavianpour M, Shekoohyian S. Comparing the efficacy of VUV and UVC/S2O82-advanced oxidation processes for degradation and mineralization of cyanide in wastewater. Chem Eng J 2016;294:273-80.
- Moussavi G, Yazdanbakhsh A, Heidarizad M. The removal of formaldehyde from concentrated synthetic wastewater using O 3/MgO/H 2 O 2 process integrated with the biological treatment. J Hazard Mater 2009;171:907-13.
- Li R, Jin X, Megharaj M, Naidu R, Chen Z. Heterogeneous fenton oxidation of 2, 4-dichlorophenol using iron-based nanoparticles and persulfate system. Chem Eng J 2015;264:587-94.
- Liu Y, He X, Fu Y, Dionysiou DD. Kinetics and mechanism investigation on the destruction of oxytetracycline by UV-254 nm activation of persulfate. J Hazard Mat 2016;305:229-39.
- Huang KC, Zhao Z, Hoag GE, Dahmani A, Block PA. Degradation of volatile organic compounds with thermally activated persulfate oxidation. Chemosphere 2005;61:551-60.
- Tsitonaki A, Petri B, Crimi M, Mosbæk H, Siegrist RL, Bjerg PL. *In* situ chemical oxidation of contaminated soil and groundwater using persulfate: A review. Crit Rev Environ Sci Technol 2010;40:55-91.
- Li Q, Sritharathikhun P, Motomizu S. Development of novel reagent for Hantzsch reaction for the determination of formaldehyde by spectrophotometry and fluorometry. Anal Sci 2007;23:413-7.
- Nash T. The colorimetric estimation of formaldehyde by means of the Hantzsch reaction. Biochem J 1953;55:416-21.
- Yang S, Wang P, Yang X, Wei G, Zhang W, Shan L. A novel advanced oxidation process to degrade organic pollutants in wastewater: Microwave-activated persulfate oxidation. J Environ Sci (China) 2009;21:1175-80.
- Wang CW, Liang C. Oxidative degradation of TMAH solution with UV persulfate activation. Chem Eng J 2014;254:472-8.
- Aslam M, Ismail IM, Salah N, Chandrasekaran S, Qamar MT, Hameed A. Evaluation of sunlight induced structural changes and their effect on the photocatalytic activity of V2O5 for the degradation of phenols. J Hazard Mater 2015;286:127-35.
- Raeisivand S, Sadeghi M, Hemati S, Fadaei A, Sedehi M. Photocatalytic degradation of catechol in aqueous solutions: a comparison between UV/Fe2O3 and Fe2O3/sunlight processes. Desalination Water Treat 2019;154:340-346.

- Lin YT, Liang C, Chen JH. Feasibility study of ultraviolet activated persulfate oxidation of phenol. Chemosphere 2011;82:1168-72.
- Ai Z, Yang P, Lu X. Degradation of 4-chlorophenol by a microwave assisted photocatalysis method. J Hazard Mater 2005;124:147-52.
- Rodriguez S, Vasquez L, Costa D, Romero A, Santos A. Oxidation of orange G by persulfate activated by Fe (II), Fe (III) and zero valent iron (ZVI). Chemosphere 2014;101:86-92.
- 23. Sidmohammadi A, Asgari G, Ebrahimi A, Sharifi Z, Movahedian AH. 4-Chlorophenol oxidation combined with the application of advanced oxidation technology and the modified microwave in chemical and petrochemical wastewater industry.Journal of Water and Wastewater 2010;6:10-20 (In Persian).
- Hettiaratchi J, Soh I, Hunte C. Practice periodical of hazardous, toxic, and radioactive waste management. Adv Solid Waste Manage Technol 2009;13:156-64.
- Wang S, Zhou N, Wu S, Zhang Q, Yang Z. Modeling the oxidation kinetics of sono-activated persulfate's process on the degradation of humic acid. Ultrason Sonochem 2015;23:128-34.
- Gao YQ, Gao NY, Deng Y, Yang YQ, Ma Y. Ultraviolet (UV) light-activated persulfate oxidation of sulfamethazine in water. Chem Eng J 2012;195:248-53.
- Gao YQ, Gao NY, Deng Y, Yin DQ, Zhang YS. Degradation of florfenicol in water by UV/Na2S2O8 process. Environ Sci Pollut Res 2015;22:8693-701.
- Esrafili A, Kalantary RR, Azari A, Ahmadi E, Gholami M. Removal of diethyl phthalate from aqueous solution using persulfate-based (UV/Na2S2O8/Fe2+) advanced oxidation process. J Mazand Univ Med Sci 2016;25:122-35.
- Saien J, Asgari H. Aqueous quinoline treatment with Iron/copper activated UV/persulfate process in a falling film photo-reactor. Iran J Chem Eng 2014;11:51.
- Zhao L, Hou H, Fujii A, Hosomi M, Li F. Degradation of 1, 4-dioxane in water with heat-and Fe2+-activated persulfate oxidation. Environ Sci Pollut Res 2014;21:7457-65.
- Guo Y, Zhou J, Lou X, Liu R, Xiao D, Fang C, *et al.* Enhanced degradation of tetrabromobisphenol A in water by a UV/base/persulfate system: Kinetics and intermediates. Chem Eng J 2014;254:538-44.
- Epold I, Trapido M, Dulova N. Degradation of levofloxacin in aqueous solutions by Fenton, ferrous ion-activated persulfate and combined fenton/persulfate systems. Chem Eng J 2015;279:452-62.
- Epold I, Dulova N. Oxidative degradation of levofloxacin in aqueous solution by S2O82–/Fe2+, S2O82–/H2O2 and S2O82–/OH – processes: a comparative study. J Env Chem Eng 2015;3:1207-14.
- 34. Sun DD, Yan XX, Xue WP. Oxidative Degradation of Dimethyl phthalate (DMP) By Persulfate Catalyzed by Ag+Combined with Microwave Irradiation. Paper Presented At: Advanced Materials Research; 2013.

6